

REMOVAL OF ZINC AND IRON METAL IONS FROM STEEL INDUSTRY EFFLUENT USING RICE HUSK AS AN ADSORBENT

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Abstract - In the ever rise dazzle race of industrialization and urbanization the earth sullied by harmful heavy metals and it is turning into a significant issue for the two researchers and masses. These heavy metals are influence straightforwardly or in a roundabout way to strength of the creatures and individuals. Effluents of industry like substance producing paper, material, treatment facility, petrochemicals, metal assembling, electro-planting, printing, color, paint, cowhide merchandise assembling, manure and pesticides and a lot more are stacked with different heavy metals and their particles. Taking into account their harmfulness, expulsion of these heavy metal particles from modern effluents has focused on the turn of events and testing of new materials. Along these lines the expulsion of heavy metals from effluents is a major issue. The adsorption procedure is generally utilized for the expulsion of overwhelming metals from emanating in view of its minimal effort, accessibility and eco-accommodating nature. Adsorption of heavy metals is another innovation for treatment of emanating containing various sorts of chosen heavy metals. Rice husk, an excess horticultural side-effect. The adsorbent rice husk is accessible as rural waste. This examination plans to assess the exhibition proficiency of the proposed adsorbent (rice husk). The adsorptive limit of rice husk for Zinc and Iron is 90.2% and 92.7% individually.

Key Words: Heavy metals, Adsorption, Adsorbent (rice husk), water treatment

1. INTRODUCTION

Pollution of air, water and soil with heavy metal is dangerous to plants, creatures and microorganism and humanity [1,2]. These poisonous metal particles are added to air, soil and water bodies from modern effluents and mining forms. These poisonous metal particles have become a genuine wellbeing peril in light of their poison levels in moderately low fixation and inclination to bioaccumulation [3,4]. Several separation techniques like precipitation, carbon adsorption, sedimentation, lime precipitation, floatation, filtration, electrochemical, natural and film forms have been accounted for to expel metal particles from wastewater. These conventional techniques have numerous disservices, for example, some of them are moderate, produce poisonous ooze [14], have helpless productivity, requires persistent contribution of synthetic compounds and include significant expense [15].

So as to conquer the previously mentioned impediments of ordinary strategies and materials, adsorption, particle trade and chelation by chelating biopolymers have generally been explored for evacuation of substantial metal particles[10]. Rice husk is the by product of the rice processing industry which is delivered in enormous amounts as a waste. Rice husk basically comprises of 35% cellulose, 25% hemicelluloses, 20% lignin, 17% debris (counting silica) and 3% rough protein[2].

Rice is most generally eaten food that satisfies the food needs of a large portion of the total populace. Different assortments of rice are developed in excess of 75 nations on the planet[5]. The yearly rice husk yield on the planet is around 500 million metric tons. Many exploration bunches have assessed unmodified rice husk for evacuation of poisonous substantial metal particles. So as to improve sorption capacities of rice husk for metal particles numerous different gatherings have utilized different adjustments of rice husk. This survey will sum up some most recent advancements utilizing rice husk and its subordinates for evacuation of heavy metal particles[8].

1.1 Chemical properties of rice husk

SiO2 - 95.3% K - 1.4% Ca - 0.7% Fe - 0.5% Other impurities – 2.1%

1.2 Physical properties of rice husk

SPECIFIC SURFACE – 186 m2/g pH – 6.0 Moisture content – 0.7% Density – 2.20 g/cm3

1.3 Sample collected area

The effluent is taken from ARADYA STEELS Pvt. Ltd. Davanagere. In this steel industry they manufacture the steel wires of different diameter. They are using water for the cooling purpose, electric arc furnaces that why waste water from steel industry contain variety of metal ions. The sample is collected with standard method and collect in plastic bottle.

2. METHODOLOGY

2.1 Adsorbent preparation

The Rice husk is washed 4 to multiple times with a refined water to evacuate all the residue and dried it at 100°C. The washed and dried rice husk is kept in the mute furnance dried at 500°C for 3 hours. At that point the powdered rice husk is taken out from the stifle furnance.

The reason for setting up the initiated rice husk (ARH) is to upgrade textural boundaries of the rice husk.100g of CRH was inundated in citric acid (0.6M) at 20°C for 2 hrs and Acid slurry is acquired. At that point Acid slurry is dried around evening time for 50°C and that dried husks is warmed at 120°C. This rice husk is washed more than once with the refined water. At last, the fine cleaned husk is broiler dried around evening time for 100°C.

2.2 Experimental Procedure for Batch Experiments

The group sorption analyze directed by shifting the mass of adsorbent. The analyses were completed in 250 ml Erlenmeyer jars and the all out volume of the response blend was kept at 100 ml. The pH of arrangement was kept up at an ideal incentive by including NaOH or HCL. Segments of the arrangement with 25 mg/l introductory fixation was set in 5 jugs, containing precisely rice husk extending in weight (0.25, 0.5, 1, 2, and 3) g with the molecule size of (0.6-1.2) mm. At that point the jugs set on a shaker and unsettled at 150 rpm constantly for 3 hours. Now the focus is in harmony. The jars were pulled back and the response blends were sifted through (Wattman 42) channels to expel any suspended adsorbent. All group tests were led at consistent temperature (25±5 C^o). Starting and last convergences of metals were dictated by nuclear ingestion spectrophotometer (AAS). The level of expulsion of substantial metals adsorption by the adsorbents was registered by utilizing the accompanying condition.

2.3 Calculation:

The amount of adsorption of heavy metal per unit mass is calculated by using the below formulae,

 $Q_{e} = \frac{(Co - Ce)V}{m}$

Where,



Co = initial concentration of heavy metal(mg/l)Ce = final concentration (mg/l)m = mass of the adsorbent (g) andV= volume of solution (L)

The % of removal of heavy metals can be calculated by,

(Co-Ce)100 % of removal = Со

3. **RESULTS AND DISCUSSION**

TABLE – 1: analysis of physicochemical parameters of steel effluent (before treatment)

| Sl.No | Parameter | Amount |
|-------|---|--------|
| 1 | рН At 25 ⁰ С | 8.9 |
| 2 | Total Dissolved Solids (Mg/L) | 958 |
| 3 | Dissolved Oxygen (% Saturation) | 19 |
| 4 | Chemical Oxygen Demand (Mg/L) | 856 |
| 5 | Biological Oxygen Demand (Mg/L) | 60 |
| 6 | Turbidity (NTU) | 23.4 |
| 7 | Conductivity (μs/Cm At 25 ⁰ C) | 1914 |
| 8 | Zn Concentration (Ppm) | 10250 |
| 9 | Fe Concentration (Ppm) | 13560 |

3.1 Effect of contact time:

1. When the adsorbent (ARH) is added to the sample. It is constructed contact with heavymetal.

2. It adsorbs the metal particles in the sample, bringing about increment the heaviness of molecule then it will be settle down.

3. The Chart – 1 and Chart – 3 shows the continuous increasing in contact time of 30min, there will be increasing in the adsorption.

3.2 Effect of adsorbent dosage:

1. The increasing in measure of adsorbent dose, increasing in the adsorption rate.

2. The Chart- 2 and Chart – 4 shows slowly increment in measure of dose of about 0.5g, the adsorption of metal particles likewise increments.

3. Maximum adsorption accurse at specific measure of dose past that there will be no increasing in adsorption rate.

4. The ARH has the adequate surface are, most extreme measure of substantial metals particles are adsorbed on the outside of the adsorbent.



For Zn

TABLE -2: Rate of Adsorption with varying contact time

| Sl. No | CO(in ppm) | Ce (in ppm) | Contact time (in | Qe (in mg/g) | % of | Dosage | pН |
|--------|------------|-------------|------------------|--------------|---------|--------|----|
| | | | min) | | removal | (in g) | |
| | | | | | | | |
| 1 | 10250 | 4868.75 | 30 | 675.6 | 52.5 | 3 | 7 |
| 2 | 10250 | 3618.25 | 60 | 828.96 | 64.7 | 3 | 7 |
| 3 | 10250 | 2757.25 | 90 | 936.59 | 73.1 | 3 | 7 |
| 4 | 10250 | 2214 | 120 | 1004.5 | 78.4 | 3 | 7 |
| 5 | 10250 | 2060.25 | 150 | 1023.7 | 79.9 | 3 | 7 |
| 6 | 10250 | 1493.75 | 180 | 1094.53 | 86.2 | 3 | 7 |
| 7 | 10250 | 1534.75 | 210 | 1089.4 | 85.0 | 3 | 7 |
| 8 | 10250 | 1520 | 240 | 1091.1 | 85.1 | 3 | 7 |



Chart - 1: Contact Time Vs % Of Removal Of Zn

| TABLE – 3: | Rate of adsorption | with varying adso | rbent dosage |
|------------|--------------------|-------------------|--------------|
|------------|--------------------|-------------------|--------------|

| Sl. No | CO(inppm) | Ce (in ppm) | Contact time (in | Qe (in | % of | Dosage | pН |
|--------|-----------|-------------|------------------|---------|---------|--------|----|
| | | | min) | mg/g) | removal | (in g) | |
| | | | | | | | |
| 1 | 10250 | 3064.75 | 180 | 1796.3 | 70.1 | 1 | 7 |
| 2 | 10250 | 2480.5 | 180 | 1294.9 | 75.8 | 1.5 | 7 |
| 3 | 10250 | 2039.75 | 180 | 1026.28 | 80.1 | 2 | 7 |
| 4 | 10250 | 1383.75 | 180 | 886.625 | 86.5 | 2.5 | 7 |
| 5 | 10250 | 1004.5 | 180 | 770.45 | 90.2 | 3 | 7 |
| 6 | 10250 | 1158.25 | 180 | 649.4 | 88.7 | 3.5 | 7 |
| 7 | 10250 | 1240.25 | 180 | 563.1 | 87.9 | 4 | 7 |
| 8 | 10250 | 1312 | 180 | 496.55 | 87.2 | 4.5 | 7 |



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Chart – 2: Adsorbent dosage vs % Of Removal of Zn

For Iron

| TABLE -4: Rate of | adsorption | with varying | contact time |
|-------------------|------------|--------------|--------------|
|-------------------|------------|--------------|--------------|

| Sl. No | CO(in | Ce (in ppm) | Contact time (in | Qe (in | % of | Dosage | pН |
|--------|-------|-------------|------------------|---------|---------|--------|----|
| | ppm) | | min) | mg/g) | removal | (in g) | |
| | | | | | | | |
| 1 | 13560 | 4705.32 | 30 | 737.89 | 65.3 | 3.5 | 7 |
| 2 | 13560 | 3878.16 | 60 | 806.82 | 71.4 | 3.5 | 7 |
| 3 | 13560 | 3308.64 | 90 | 854.28 | 75.6 | 3.5 | 7 |
| 4 | 13560 | 2671.32 | 120 | 907.39 | 80.3 | 3.5 | 7 |
| 5 | 13560 | 1396.68 | 150 | 1013.61 | 89.7 | 3.5 | 7 |
| 6 | 13560 | 1084.8 | 180 | 1039.6 | 92 | 3.5 | 7 |
| 7 | 13560 | 1166.16 | 210 | 1032.82 | 91.4 | 3.5 | 7 |
| 8 | 13560 | 1098.36 | 240 | 1038.47 | 91.9 | 3.5 | 7 |







| Sl. No | CO(in | Ce (in | Contact time (in | Qe (in | % of | Dosage | pН |
|--------|-------|---------|------------------|---------|---------|--------|----|
| | ppm) | ppm) | min) | mg/g) | removal | (in g) | |
| 1 | 13560 | 5057.88 | 180 | 2125.53 | 62.7 | 1 | 7 |
| 2 | 13560 | 4040.88 | 180 | 1586.52 | 70.2 | 1.5 | 7 |
| 3 | 13560 | 3159.48 | 180 | 1300.06 | 76.7 | 2 | 7 |
| 4 | 13560 | 1708.56 | 180 | 1185.14 | 87.4 | 2.5 | 7 |
| 5 | 13560 | 1328.88 | 180 | 1019.26 | 90.2 | 3 | 7 |
| 6 | 13560 | 949.2 | 180 | 900.77 | 93 | 3.5 | 7 |
| 7 | 13560 | 962.76 | 180 | 787.39 | 92.9 | 4 | 7 |
| 8 | 13560 | 1193.28 | 180 | 687.04 | 91.2 | 4.5 | 7 |

TABLE – 5: Rate of adsorption with varying the adsorbent dosage



Chart -4: adsorbent dosage vs % Of Removal Of Fe

4. CONCLUSIONS

This examination is take on to investigate the adsorption of Zinc and Iron on rice husk-based adsorbents i.e., actuated rice husk (ARH). In view of this outcomes taken out from the tests, the accompanying end were down.

- 1. Here the rice husk is minimal effort adsorbent. Gotten from the rice factory or horticultural land. The treated rick husk (ARH) has more adsorption capacity than the untreated one.
- 2. From the got outcome we inferred that heavy metals like Zinc and Iron are expelled from the steel gushing utilized ARH given more productivity.
- 3. The outcome shows that evacuation productivity will increment with increment in pH, measurements, contact time. The most extreme heavy metals are adsorbed at specific point past that it is steady.
- 4. The heavy metals expelling in the examples utilizing ARH as an adsorbent in the cluster analyze gives that net take-up of the Zinc and Iron is 90.2% and 92.7% separately. Along these lines, it is inferred that ARH is known for its higher potential to evacuate the heavy metals which is available in the sample gushing of steel industry.

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